WHAT IS CLAIMED IS:

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1. A method of coating a CMC fiber, comprising:

passing said fiber through a reaction zone along a path substantially parallel to a longitudinal axis of said zone,

passing a flow of fiber coating reactant though said reaction zone; and

- disrupting at least a portion of said flow of reactant from a path substantially parallel to said fiber path to create a mixing flow adjacent said fiber.
 - 2. The method of claim 1, wherein said reaction zone is a CVD reactor chamber.
- 3. The method of claim 2, wherein said fiber is passed through a first seal through said CVD reactor chamber to discharge at a second seal of said reactor chamber.
 - 4. The method of claim 1, wherein said fiber comprises a single monofilament fiber.
 - 5. The method of claim 1, wherein said fiber comprises a fiber tow.
 - 6. The method of claim 5, wherein a plurality of fiber tows are simultaneously passed through said reaction zone for coating.
 - 7. The method of claim 1, wherein said fiber is a silicon carbide fiber.
- 20 8. The method of claim 1, wherein said fiber is an aluminum oxide fiber.
 - 9. The method of claim 1, wherein said fiber is a silicon carbide-based fiber.

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- 10. The method of claim 1, wherein said fiber coating reactant comprises a hydrocarbon.
- The method of claim 1, wherein said fiber coating reactant comprises methane.
- 12. The method of claim 1, wherein said fiber coating reactant comprises boron trichloride and ammonia.
 - 13. The method of claim 1, wherein said fiber coating reactant comprises boron trichloride, ammonia and a silicon precursor.
- 14. The method of claim 13, wherein the silicon precursor is selected from dichlorosilane, trichlorosilane, silicon tetrachloride and silane.
 - The method of claim 1, wherein said fiber coating reactant includes hydrogen or nitrogen.
 - 16. The method of claim 1, wherein said reaction zone is maintained at a pressure about 0.05 Torr to about atmospheric pressure (760 Torr).
 - The method of claim 1, wherein said reaction zone is maintained at a pressure about 0.1 to about 50 Torr.
 - 18. The method of claim 1, wherein said reaction zone is maintained at a pressure about 0.3 to about 10 Torr.
 - .19 The method of claim 1, wherein said reaction zone is maintained at temperature of about 700° to about 1800°C.
 - 20. The method of claim 1, wherein said reaction zone is maintained at temperature of about 1100° to about 1550°C.
 - 21. The method of claim 1, wherein said reaction zone is maintained at temperature of about 1350° to about 1500°C.

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- 22. The method of claim 1, wherein a tow of fibers is passed through the reaction zone and the tows are spaced apart about 0.020 to about 1 inch.
- 23. The method of claim 1, wherein a tow of fibers is passed through the reaction zone and the tows are spaced apart about 0.045 to about 0.25.
- 24. The method of claim 1, wherein a tow of fibers is passed through the reaction zone and the tows are spaced apart about 0.05 to about 0.1 inch.
- 25. The method of claim 1, the fiber is passed through the reaction zone at a rate from about 1 to about 200 inches/minute.
- The method of claim 1, the fiber is passed through the reaction zone at a rate from 5 to about 100 inch/minute.
 - 27. The method of claim 1, the fiber is passed through the reaction zone at a rate from about 10 to about 60 inches/minute.
 - 28. A coating reactor, comprising:

a reactor chamber to accommodate a fiber passing along a path substantially parallel to a longitudinal axis of said chamber and a flow of fiber coating reactant; and

a flow disrupter located within said reactor chamber to disrupt at least a portion of said flow of reactant from a path substantially parallel to said fiber path to create a mixing flow adjacent said fiber.

- 29. The coating reactor of claim 28, wherein said reactor chamber is a CVD reactor chamber.
- 30. The coating reactor of claim 29, wherein said CVD reactor chamber has a first seal to admit said flow of reactant and a second seal to discharge said flow of reactant.

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- 31. The coating reactor of claim 30, further comprising a first fiber aperture through which said fiber can be pulled to enter the reactor chamber and a second aperture to allow exit of the fiber from the reactor chamber.
- 32. The coating reactor of claim 28, wherein said disrupter comprises a disrupter face angled about 10° to about 90° from said longitudinal axis of the reactor in a direction against said flow of reactant.
- 33. The coating reactor of claim 28, wherein said disrupter comprises a disrupter face angled about 15° to about 50° from said longitudinal axis of the reactor in a direction against said flow of reactant.
- 34. The coating reactor of claim 28, wherein said disrupter comprises a plurality of structures mounted intermittently along an inside wall of said reactor chamber.
- 35. The coating reactor of claim 28, wherein said disrupter comprises a forward angled face and a following angled face.
- 36. The coating reactor of claim 28, wherein said disrupter comprises a forward face that is angled 90 form said longitudinal axis of the reactor.
 - 37. A coating reactor, comprising:

a reactor chamber to accommodate a fiber passing along a path substantially parallel to a longitudinal axis of said chamber and a flow of fiber coating reactant; and

a plurality of reactant injection inlets intermittently spaced along said longitudinal axis of said chamber and directed into said chamber at an angle to said fiber to create a mixing flow adjacent said fiber.

38. The reactor of claim 37, wherein said inlets are offset from each other along said longitudinal axis.

39. A coating reactor, comprising:

a reactor chamber to accommodate a fiber; and

a set of rollers along the interior of said chamber to convey the fiber tow repeatedly back and forth across the reactor longitudinal axis to interact with the reactant gas flow.